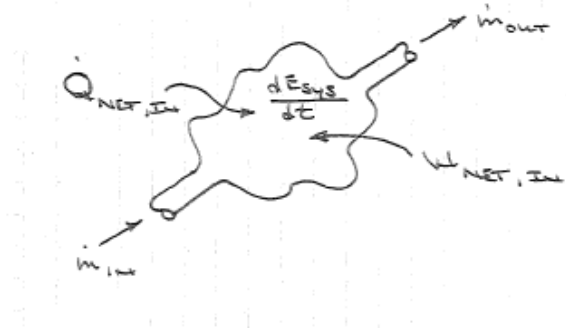


## Control Volume Analysis

So far, our derivation of the energy balance equation has been limited to closed systems.

Let us now develop a generalized energy balance for open systems or Control Volumes.



In open systems, there is mass flow across the control volume boundary.

CONSERVATION OF MASS : FOR A CONTROL VOLUME

$$\left[ \begin{array}{c} \text{RATE OF} \\ \text{CHANGE} \\ \text{OF MASS} \\ \text{IN C.V.} \end{array} \right] = \left[ \begin{array}{c} \text{MASS FLOW RATE} \\ \text{ENTERING} \\ \text{C.V.} \end{array} \right] - \left[ \begin{array}{c} \text{MASS FLOW RATE} \\ \text{LEAVING} \\ \text{C.V.} \end{array} \right]$$

$$\frac{dm_{cv}}{dt} = \sum \dot{m}_i - \sum \dot{m}_e \quad \left[ \frac{kg}{s} \right]$$

Since energy is conserved across the control volume, we must account for the energy accompanying the mass.

Total mass in the control volume at an instant is

$$m_{cv}(t) = \int_V \rho dV$$

Where:

- $v_n$  = component of the relative velocity normal to  $dA$  in the direction of flow

Mass flow rate,  $\dot{m}$ , entering or exiting the control volume is

$$\left[ \begin{array}{c} \text{amount of mass crossing } dA \\ \text{during the time interval } \Delta T \end{array} \right] = \rho(v_n \Delta T) dA$$

$$\rho(v_n \Delta T) dA = \left[ \frac{kg}{m^3} \right] \left[ \frac{m}{s} \right] [s] [m^2] = [kg]$$

Divide both sides by  $\Delta T$

$$\left[ \begin{array}{l} \text{instantaneous mass flow} \\ \text{rate across } dA \end{array} \right] = \rho v_n dA$$

Integrate across all of area,  $A$

$$\dot{m} = \int_A \rho v_n dA$$

In one dimensional flow:  $\dot{m} = \rho A v = \frac{A v}{v}$

## Conservation of Energy for a Control Volume

$$\left[ \begin{array}{l} \text{Change of energy} \\ \text{in CV} \end{array} \right] = \left[ \begin{array}{l} \text{Energy} \\ \text{entering CV} \end{array} \right] - \left[ \begin{array}{l} \text{Energy} \\ \text{leaving CV} \end{array} \right]$$

$$\Delta(u + KE + PE)_{cv} = Q - W + \dot{m}_i \left( u_i + \frac{v_i^2}{2} + gz_i \right) - \dot{m}_e \left( u_e + \frac{v_e^2}{2} + gz_e \right)$$

Time rate energy balance

$$\frac{dE_{cv}}{dt} = \dot{Q} - \dot{W} + \dot{m}_i \left( u_i + \frac{v_i^2}{2} + gz_i \right) - \dot{m}_e \left( u_e + \frac{v_e^2}{2} + gz_e \right)$$

## Work in a Control Volume

There are two contributions to the work term  $\dot{W}$

$$\dot{W} = \dot{W}_p + \dot{W}_{cv}$$

1.  $\dot{W}_p$  = Work associated with the fluid pressure as mass is introduced at inlets and removed at exits
2.  $\dot{W}_{cv}$  = All other work effects associated with rotating shafts, displacement of the boundary, electrical, magnetic, etc.

Rate of energy transfer by work = force x velocity ( $W = F \cdot d$ )

$$\text{flow work at the exit} = \left[ \begin{array}{l} \text{Time rate of energy transfer} \\ \text{by work from the control} \\ \text{volume at exit} \end{array} \right] = (p_e A_e) v_e$$

Where:

- $p_e$  is the pressure of the flowing matter at exit

Therefore

$$\dot{W} = \dot{W}_{cv} + (p_e A_e)v_e - (p_i A_i)v_i$$

or since  $Av = \dot{m}v$ , where  $v$  is the specific volume, this can be rewritten:

$$\dot{W} = \dot{W}_{cv} + \dot{m}_e(p_e v_e) - \dot{m}_i(p_i v_i)$$

Substituting these new work components into the energy balance yields

$$\frac{dE_{cv}}{dt} = \dot{Q}_{cv} - \dot{W}_{cv} + \dot{m}_i \left( u_i + p_i v_i + \frac{v_i^2}{2} + gz_i \right) - \dot{m}_e \left( u_e + p_e v_e + \frac{v_e^2}{2} + gz_e \right)$$

## Enthalpy

The sum of the internal energies,  $u$ , and flow work. It is often expressed in its per unit mass form, as presented in the energy balance

$$h = u + pv$$

Substituting enthalpy into the energy balance, we get the general form of the 1st law energy balance

$$\frac{dE_{cv}}{dt} = \dot{Q}_{cv} - \dot{W}_{cv} + \dot{m}_i \left( h_i + \frac{v_i^2}{2} + gz_i \right) - \dot{m}_e \left( h_e + \frac{v_e^2}{2} + gz_e \right)$$

Remember if steady state,  $\frac{dE_{cv}}{dt} = 0$ , and  $\dot{m}_i = \dot{m}_e$ ,

Therefore the steady state energy balance may be expressed as:

$$\frac{\dot{Q}_{cv}}{\dot{m}} - \frac{\dot{W}_{cv}}{\dot{m}} + (h_i - h_e) + \frac{v_i^2 - v_e^2}{2} + g(z_i - z_e) = 0$$