



### Radiation Heat Transfer in Two-Surface Enclosures

Consider an enclosure consisting of two opaque surfaces at specified temperatures  $T_1$  and  $T_2$ , as shown in Fig. 22–24, and try to determine the net rate of radiation heat transfer between the two surfaces with the network method. Surfaces 1 and 2 have emissivities  $\epsilon_1$  and  $\epsilon_2$  and surface areas  $A_1$  and  $A_2$  and are maintained at uniform temperatures  $T_1$  and  $T_2$ , respectively. There are only two surfaces in the enclosure, and thus we can write

$$\dot{Q}_{12} = \dot{Q}_1 = -\dot{Q}_2$$

That is, the net rate of radiation heat transfer from surface 1 to surface 2 must equal the net rate of radiation heat transfer *from* surface 1 and the net rate of radiation heat transfer *to* surface 2.

The radiation network of this two-surface enclosure consists of two surface resistances and one space resistance, as shown in Fig. 22–24. In an electrical network, the electric current flowing through these resistances connected in series would be determined by dividing the potential difference between points *A* and *B* by the total resistance between the same two points. The net rate of radiation transfer is determined in the same manner and is expressed as

$$\dot{Q}_{12} = \frac{E_{b1} - E_{b2}}{R_1 + R_{12} + R_2} = \dot{Q}_1 = -\dot{Q}_2$$

or

$$\dot{Q}_{12} = \frac{\sigma(T_1^4 - T_2^4)}{\frac{1 - \epsilon_1}{A_1 \epsilon_1} + \frac{1}{A_1 F_{12}} + \frac{1 - \epsilon_2}{A_2 \epsilon_2}} \quad (\text{W}) \quad (22-36)$$

This important result is applicable to any two gray, diffuse, and opaque surfaces that form an enclosure. The view factor  $F_{12}$  depends on the geometry and must be determined first. Simplified forms of Eq. 22–36 for some familiar arrangements that form a two-surface enclosure are given in Table 22–3. Note that  $F_{12} = 1$  for all of these special cases.

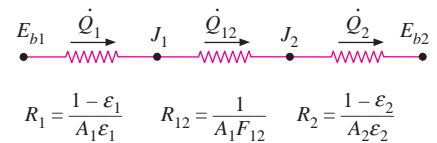
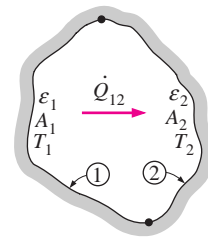


FIGURE 22–24

Schematic of a two-surface enclosure and the radiation network associated with it.

#### EXAMPLE 22–7 Radiation Heat Transfer between Parallel Plates

Two very large parallel plates are maintained at uniform temperatures  $T_1 = 800$  K and  $T_2 = 500$  K and have emissivities  $\epsilon_1 = 0.2$  and  $\epsilon_2 = 0.7$ , respectively, as shown in Fig. 22–25. Determine the net rate of radiation heat transfer between the two surfaces per unit surface area of the plates.

**SOLUTION** Two large parallel plates are maintained at uniform temperatures. The net rate of radiation heat transfer between the plates is to be determined.

**Assumptions** Both surfaces are opaque, diffuse, and gray.

**Analysis** The net rate of radiation heat transfer between the two plates per unit area is readily determined from Eq. 22–38 to be

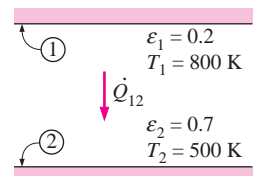
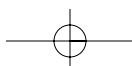


FIGURE 22–25

The two parallel plates considered in Example 22–7.



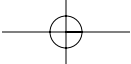
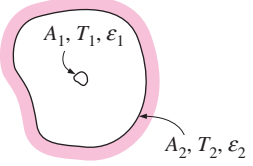
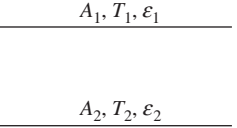
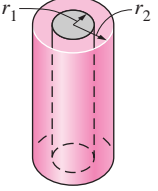
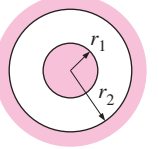


TABLE 22-3

<p>Small object in a large cavity</p> 	$\frac{A_1}{A_2} \approx 0$ $F_{12} = 1$	$\dot{Q}_{12} = A_1 \sigma \varepsilon_1 (T_1^4 - T_2^4) \quad (22-37)$
<p>Infinitely large parallel plates</p> 	$A_1 = A_2 = A$ $F_{12} = 1$	$\dot{Q}_{12} = \frac{A \sigma (T_1^4 - T_2^4)}{\frac{1}{\varepsilon_1} + \frac{1}{\varepsilon_2} - 1} \quad (22-38)$
<p>Infinitely long concentric cylinders</p> 	$\frac{A_1}{A_2} = \frac{r_1}{r_2}$ $F_{12} = 1$	$\dot{Q}_{12} = \frac{A_1 \sigma (T_1^4 - T_2^4)}{\frac{1}{\varepsilon_1} + \frac{1 - \varepsilon_2}{\varepsilon_2} \left(\frac{r_1}{r_2}\right)} \quad (22-39)$
<p>Concentric spheres</p> 	$\frac{A_1}{A_2} = \left(\frac{r_1}{r_2}\right)^2$ $F_{12} = 1$	$\dot{Q}_{12} = \frac{A_1 \sigma (T_1^4 - T_2^4)}{\frac{1}{\varepsilon_1} + \frac{1 - \varepsilon_2}{\varepsilon_2} \left(\frac{r_1}{r_2}\right)^2} \quad (22-40)$

$$\begin{aligned} \dot{q}_{12} &= \frac{\dot{Q}_{12}}{A} = \frac{\sigma (T_1^4 - T_2^4)}{\frac{1}{\varepsilon_1} + \frac{1}{\varepsilon_2} - 1} = \frac{(5.67 \times 10^{-8} \text{ W/m}^2 \cdot \text{K}^4)[(800 \text{ K})^4 - (500 \text{ K})^4]}{\frac{1}{0.2} + \frac{1}{0.7} - 1} \\ &= 3625 \text{ W/m}^2 \end{aligned}$$

**Discussion** Note that heat at a net rate of 3625 W is transferred from plate 1 to plate 2 by radiation per unit surface area of either plate.

